

ChE 374–Lecture 6–Mass Balance

- Reynolds Transport Theorem: $\frac{dB_{sys}}{dt} = \frac{d}{dt} \int_{CV} \rho b dV + \int_A \rho b \vec{v} \cdot \vec{n} dA$.

$\rho b \vec{v} \cdot \vec{n}$ is the flux of B stuff through the control surface.

- Integral Mass Balance

1. $B = M$, $b = B/M = 1$.
2. Apply the conservation law: $dM/dt = 0$: mass is conserved.
3. $\frac{d}{dt} \int_{CV} \rho dV + \int_A \rho \vec{v} \cdot \vec{n} dA = 0$.

- Cases

1. Steady State
2. Constant density
 - * Liquids have approximately constant density
 - * Gas density: ideal gas law: vary pressure (high speed flows or compressor), vary temperature (e.g., combustion), vary moles (e.g., combustion/reaction).
3. Uniform inside C.V. and/or Uniform inlet/outlet flows over surface.
4. Fixed or variable C.V. The control volume C.V. can move
 - * $\vec{v} = \vec{v}_{sys} - \vec{v}_{cv}$.
 - * Can pull the d/dt inside the integral.

$$\frac{dm}{dt} = \dot{m}_{in} - \dot{m}_{out}$$

- Examples

- Simple flow with change in area of inlet/outlet.
 - * Fixed CV, SS, Constant ρ , Uniform Flows.
- Filling a tank with inlet and outlet.
 - * Constant ρ , Uniform Flows, not S.S., none-fixed C.V.
- Nonuniform flow \rightarrow compute the average velocity from a velocity profile.

- Differential Form of Mass Balance.

- Get from the Integral form with a small/uniform property control volume and shrink to a point.
- Get from the Gauss Divergence Theorem.

Class 6 - Integral Mass Balance.

(1)

$$\text{R.T.T. : } \frac{dB_{\text{sys}}}{dt} = \frac{d}{dt} \int_{CV} \rho b dV + \int_{CS} \rho \vec{v} \cdot \vec{n} dA$$

Integral Mass Balance.

$$\textcircled{1} \quad B = M \quad (\text{kg})$$

$$b = \frac{B}{M} = 1$$

$$\rightarrow \frac{dM}{dt} = \frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho \vec{v} \cdot \vec{n} dA$$

② Apply Conservation

$$\text{Law } \frac{dM}{dt} = 0$$

$$\rightarrow \boxed{\frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho \vec{v} \cdot \vec{n} dA = 0}$$

That's it!

Cases

① S.S. \rightarrow nothing changes at a given point
 $\frac{d}{dt} \int_{CV} \rho dV = \frac{dM_{CV}}{dt} = 0$ at S.S.

$$\rightarrow \int_{CS} \rho \vec{v} \cdot \vec{n} dA = 0$$

② Const ρ \rightarrow \div through by ρ , $\int_{CV} dV = V$

$$\rightarrow \frac{dV_{CV}}{dt} + \int_{CS} \vec{v} \cdot \vec{n} dA = 0$$

if the C.V. is fixed then $\int_{CS} \vec{v} \cdot \vec{n} dA = 0$

• Liq: $\rho \sim \text{const.}$

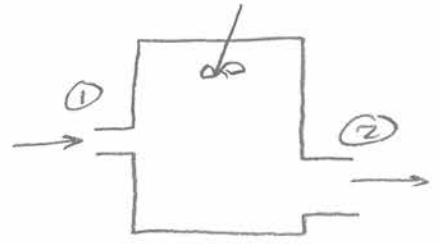
• Gases $P = MP/RT \rightarrow P, T, M$ vary

• High Speed flow \rightarrow high ΔP

• Reactions $\rightarrow \Delta T, \Delta n_{\text{mols}} \rightarrow \Delta M$

• For low speed, \sim Isothermal, $\rho_{\text{gas}} \approx \text{const.}$

③ Uniform Props inside C.V.
Uniform inlets, outlets



$$\frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho \vec{V} \cdot \vec{n} dA = 0$$

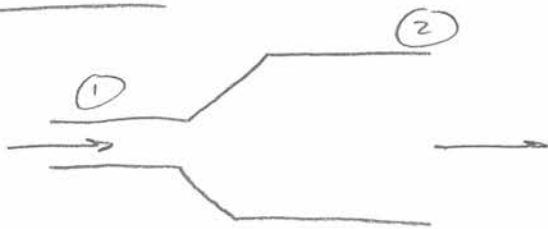
$$\frac{d\rho V}{dt} + (PVA)_{out} - \underbrace{(PVA)_{in}}_{\dot{m}} = 0$$

$\vec{V} \cdot \vec{n}$ @ ① is neg
 $\vec{V} \cdot \vec{n}$ @ ② is pos

$$\frac{dM_{cv}}{dt} = \dot{m}_{in} - \dot{m}_{out}$$

V, ρ can change in time.

Example 1



Water, S.S.

- Q: Fixed C.V. → Y
- Q: SS → Y
- Q: Const P → Y
- Q: Unif inlet → Y

SS. → $\int_{CS} \rho \vec{V} \cdot \vec{n} dA = 0$

Const P → $\int_{CS} \vec{V} \cdot \vec{n} dA = 0$

Uniform → $V_2 A_2 - V_1 A_1 = 0$

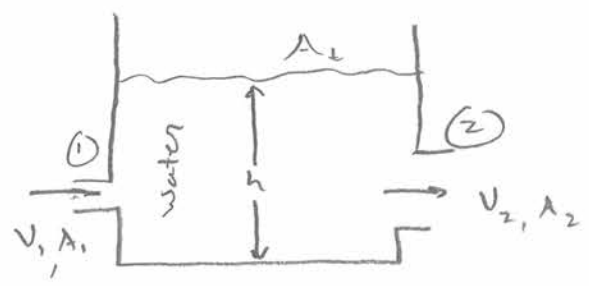
or $V_2 A_2 = V_1 A_1$
or $(PAV)_1 = (PAV)_2$

→ $\dot{m}_{in} = \dot{m}_{out}$
or $\dot{V}_{in} = \dot{V}_{out}$

$$V_2 = V_1 \frac{A_1}{A_2}$$

Volume flow in = Volume flow out.

Example 2 : Given V_1, V_2, A_1, A_2, A_t
Find $h(t)$



- Q: Fixed C.V. ? \rightarrow N
- Take C.V. = water in Tank
- Q: Const ρ ? \rightarrow Y
- Q: Uniform ? \rightarrow Y
- Q: SS ? \rightarrow N

Const $\rho \rightarrow \frac{d\mathcal{V}}{dt} + \int_{\mathcal{V}} \vec{v} \cdot \vec{n} dA = 0$

Unif $\rightarrow \frac{d\mathcal{V}}{dt} + V_2 A_2 - V_1 A_1 = 0$

$\mathcal{V} = A_t h$, \rightarrow \div by A_t , rearrange

$$\frac{dh}{dt} = \underbrace{\left(\frac{V_1 A_1 - V_2 A_2}{A_t} \right)}_{\text{Const } C}$$

Solve $\rightarrow h = h_0 + \left(\frac{V_1 A_1 - V_2 A_2}{A_t} \right) t$

Suppose $V = V(h)$?
 $V = V(t)$?

insert in ODE then solve ODE

* Always Try to align The C.V. , C.S. to be \perp to The Velocities

Example : Nonuniform Flow

$$\dot{\mathcal{V}} = \int v dA \rightarrow d\dot{\mathcal{V}} = v dA \rightarrow \dot{\mathcal{V}} = \int v dA$$

$$\bar{V} = \frac{1}{A} \int v dA \rightarrow \dot{\mathcal{V}} = \int v dA = A \bar{V}$$

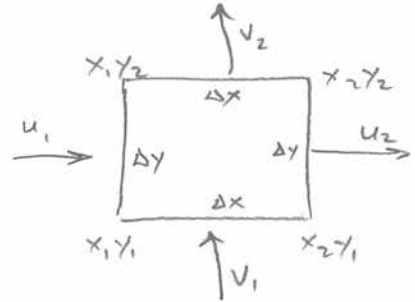
Given a velocity profile, Find $\bar{V} = \frac{1}{A} \int v(x) dA$

- Plug in given $v(x)$, set dA , such as $dA = w dx$
- Integrate.

Differential Mass Balance.

Fixed C.V., uniform

$$\frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho \vec{v} \cdot \vec{n} dA = 0$$



$$\cancel{\Delta x \Delta y} \frac{d\rho}{dt} + \rho_{x_2} u_2 \Delta y - \rho_{x_1} u_1 \Delta y + \rho_{y_2} v_2 \Delta x - \rho_{y_1} v_1 \Delta x = 0$$

• here Areas are $\Delta x, \Delta y$ for a unit Δz in the Page.

$$\div \Delta x, \Delta y \rightarrow \frac{d\rho}{dt} + \frac{\rho_{x_2} u_2 - \rho_{x_1} u_1}{\Delta x} + \frac{\rho_{y_2} v_2 - \rho_{y_1} v_1}{\Delta y} = 0$$

$$\lim_{\Delta x, \Delta y \rightarrow 0} \rightarrow \frac{\partial \rho}{\partial t} + \frac{\partial \rho u}{\partial x} + \frac{\partial \rho v}{\partial y} = 0$$

$$\rightarrow \boxed{\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{v}) = 0}$$

Optional

Gauss Divergence Theorem (GDT)

$$\int_A \vec{v} \cdot \vec{n} dA = \int_{CV} \nabla \cdot \vec{v} dV \quad \equiv \text{GDT}$$

$$\text{Then } \frac{d}{dt} \int_{CV} \rho dV + \int_{CS} \rho \vec{v} \cdot \vec{n} dA = 0$$

$$\rightarrow \frac{d}{dt} \int_{CV} \rho dV + \int_{CV} \nabla \cdot (\rho \vec{v}) dV = 0$$

$$\rightarrow \int_{CV} \left(\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{v}) \right) dV = 0$$

$$\rightarrow \boxed{\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \vec{v}) = 0}$$