

## ChE 374–Lecture 37–Compressible Flows

- Compressible flows occur at high speeds (B.E.  $\Delta P = 1/2\rho\Delta v^2$ .)
  - Gas can convert significant internal energy to kinetic energy.
  - Density decreases, temperature decreases.
  - Mach number:  $\mathcal{M} = v/c$ , where  $c$  is the *local* speed of sound.
  - Compressible flow for  $\mathcal{M} > 0.3 \rightarrow$  density ratio  $\approx 0.95 \rightarrow$  5% difference.
    - \* Most scalings go with  $\mathcal{M}^2$ .
- Sound Speed
  - Follow a pressure pulse (frame of the pulse).
    - \* Mass balance ( $\rho Av$ ) and momentum balance (pressure force, flow in, flow out) give (for ideal gases):

$$v = \sqrt{\left(\frac{\partial P}{\partial \rho}\right)_s} = c = \sqrt{\frac{kRT}{M}},$$

where  $k = C_P/C_V$ , and  $M$  is the mean molecular weight.

- Values for air:
  - \*  $k = 1.4$
  - \* Air at 25 C = 77 F:  $c = 346 \text{ m/s} = 774 \text{ mph}$
  - \* Air at 2000 K = 3140 F:  $c = 896 \text{ m/s} = 2000 \text{ mph}$ 
    - (heavier gases give slower speed, and higher temperatures give higher speed).
- Water at 15 C  $c = 1490 \text{ m/s} = 3333 \text{ mph}$ .
- Steel at 15 C  $c = 5060 \text{ m/s} = 11318 \text{ mph}$ .
- Analysis: SS, no friction, 1D, Ideal Gas
  - Energy balance from a reservoir into some pipe/valve/etc.
    - \* No heat, no shaft work, no gravity effect,  $P/\rho + u = h$ , and  $dh = C_p dT$ .  
Use definition of  $k$ , and  $c$  given above to obtain:

$$\frac{T_r}{T_1} = \frac{\mathcal{M}_1^2(k-1)}{2} + 1,$$

where  $r$  denotes the reservoir (no velocity), and subscript 1 is the point of interest.

- For ideal gases:  $P_r/P_1 = (T_r/T_1)^{k/(k-1)}$ ,  $\rho_r/\rho_1 = (T_r/T_1)^{1/(k-1)}$ . So:

$$\frac{P_r}{P_1} = \left( \mathcal{M}^2 \frac{k-1}{2} + 1 \right)^{k/(k-1)}$$

$$\frac{\rho_r}{\rho_1} = \left( \mathcal{M}^2 \frac{k-1}{2} + 1 \right)^{1/(k-1)}$$

- Flow in nozzles.
  - For incompressible flow, the density is constant and have  $\dot{m} = \rho Av$ .
  - For compressible flow, the density drops. For  $\mathcal{M} < 1$ , the density drops slower than velocity increases for a given change in area and we need a converging nozzle as usual to increase the velocity through the nozzle. For  $\mathcal{M} > 1$ , the density drops faster than velocity increases for a given change in area and we need a *diverging* nozzle to increase the velocity through the nozzle. Hence the converging/diverging nozzles on rockets.
- Choked Flow: Pressure ratios below 0.53, result in choked flow in valves, etc. For choked flow, there is a maximum flow rate, independent of what is done downstream.
  - Most control valves, safety valves, bike tire valves are choked.
  - **YOU MUST KNOW AND UNDERSTAND THIS CONCEPT**

# Class 37 - Compressible Flows

Previously: Const  $\rho$ .

Now,  $\rho$  varies

- High Speed flow, large  $\Delta P$ ,  $\Delta V$ ,  $\Delta T$ , etc.
- Gas converts internal energy to kinetic energy
  - T Drops ;  $\rho$  Drops
  - $V >$  Bernoulli eqn where  $\rho$  is const.
- Mach number  $M = V/c$  ;  $c$  is the local value  
since  $c$  varies with temperature,
- Compressible for  $M > 0.3 \rightarrow \frac{P}{P} \sim 0.95 \rightarrow 5\%$
- Most Scalings Go with  $M^2$

## Sound Speed

Follow a pressure Pulse



- Ride the pulse  $\rightarrow$  Flow in/out of C.V. moving at Sound Speed:  $c$

Mass Balance:  $\dot{m} = \dot{m} \rightarrow \rho A V = (\rho + d\rho) A (V + dV)$

$$\rightarrow \cancel{\rho V} = \cancel{\rho V} + \rho dV + V d\rho + \cancel{d\rho dV}$$

ignore

$$\rightarrow \boxed{\rho dV = -V d\rho}$$

Momentum Balance: SS, only Pressure forces

$$AP - A(P + dP) = \dot{m}(V + dV) - \dot{m}V$$

$\dot{m} = \rho A V$ ,  $A$  cancels.

$$-dP = \rho V dV \rightarrow \boxed{\rho dV = -\frac{dP}{V}}$$

insert

Insert  $\rho dV = -v d\rho$  from Mass Bal

$$\frac{dP}{d\rho} = v^2 = c^2 \rightarrow c = \sqrt{\frac{dP}{d\rho}} \rightarrow$$

•  $P = \frac{\rho RT}{M}$  ;  $\frac{dP}{d\rho} \rightarrow \left(\frac{\partial P}{\partial \rho}\right)_T$  or  $\left(\frac{\partial P}{\partial \rho}\right)_s$

• Sound waves Compress  $\rightarrow$  no heat transfer  $\rightarrow$  isentropic, But

•  $c = \sqrt{\left(\frac{\partial P}{\partial \rho}\right)_s} = \sqrt{\frac{kRT}{M}} = c$  not isothermal,

•  $k = C_p/C_v$

•  $k = 1.4$  for Air

	$c$ (m/s)	$c$ (mph)
Air @ 298k	346	774
Air @ 2000k	896	2000
H <sub>2</sub> O @ 15°C	1490	3333
Steel @ 15°C	5060	11318

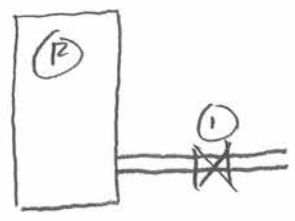
• Note:  $\left(\frac{\partial P}{\partial \rho}\right)_T = \frac{RT}{M} \rightarrow$  off by  $\sqrt{k} = 18\%$  or  $84\%$

### Analysis

- Take Flow from some Large Reservoir,  $v \approx 0$ .
- Also called Stagnation Condition Corresponding to a Given Flow.
- This is a Convenient Reference State,

• Assume: S.S., 1-D, Ideal Gas, no friction, ignore Gravity

• Energy Balance:  $\dot{Q} + \dot{w}_s = \dot{m} \left( \underbrace{\frac{P}{\rho}}_h + u + \frac{v^2}{2} + g/z \right)_2 - \dot{m} \left( \frac{P}{\rho} + u + \frac{v^2}{2} + g/z \right)_1$



$$\rightarrow v_1^2 = 2(h_r - h_1)$$

$$= 2C_p(T_r - T_1)$$

Now :  $C_p = C_v + \frac{R}{M}$

$k = C_p/C_v \rightarrow C_v = C_p/k$

$C_p = \frac{C_p}{k} + \frac{R}{M} \rightarrow C_p = \frac{Rk}{M(k-1)}$

→ insert above

$V_1^2 = \frac{2(Rk)}{M(k-1)} (T_r - T_1)$

use  $C^2 = \frac{kRT}{M}$

$\frac{V_1^2}{C_1^2} = M^2 = \frac{2}{k-1} \left( \frac{T_r}{T_1} - 1 \right)$

→  $\frac{T_r}{T_1} = \frac{M^2 (k-1)}{2} + 1$

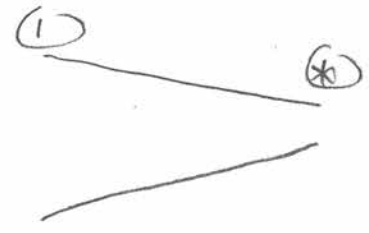
For ideal Gases (see Thermo Class next Semester)

$\frac{P_r}{P_1} = \left( \frac{T_r}{T_1} \right)^{k/(k-1)} ; \frac{P_r}{P_1} = \left( \frac{T_r}{T_1} \right)^{\frac{1}{k-1}}$

Then, using  $\frac{T_r}{T_1}$  above,

$\frac{P_r}{P_1} = \left( M^2 \frac{k-1}{2} + 1 \right)^{\frac{k}{k-1}}$   
 $\frac{P_r}{P_1} = \left( M^2 \frac{k-1}{2} + 1 \right)^{\frac{1}{k-1}}$

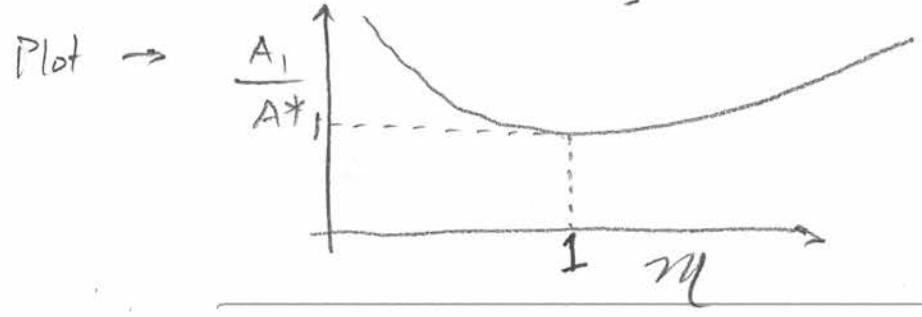
# Nozzles.



$\dot{m} = \rho A V = \text{const}$   
 As  $A$  Decreases  $V$  increases,  
 Eventually  $V = C$  at (\*)

$\frac{A_1}{A^*} = \frac{\rho^* V^*}{\rho_1 V_1}$  ; insert  $\rho = \rho_R \left[ M^2 \frac{k-1}{2} + 1 \right]^{-\frac{1}{k-1}}$   
 (note that our reference Reservoir Condition  $\rho_R$  cancels). Note  $M$  at (\*) = 1

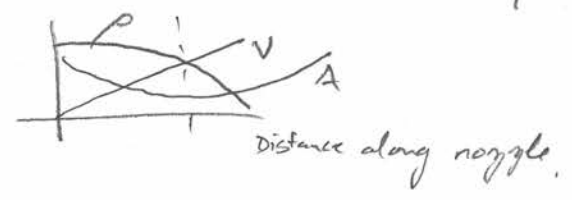
\*  $\frac{A_1}{A^*} = \frac{1}{M_1} \left[ \frac{M_1^2 \frac{(k-1)}{2} + 1}{\frac{(k-1)}{2} + 1} \right]^{\frac{(k+1)}{2(k-1)}}$



For  $M < 1$ , As velocity increases,  $A$  Decreases.

For  $M > 1$ , As velocity increases,  $A$  increases!

- Because  $\rho$  is Decreasing Faster Than  $A$  is Decreasing  $\rightarrow V$  increases to keep  $\dot{m} = \rho A V$  Constant.



# Choked Flow.

Consider a Nozzle



- Start with high P in a Reservoir and Drop the pressure outside.
- Velocity increases in nozzle till hit Sonic Velocity,  $M=1$
- At that point, further reduction cannot be communicated upstream
- If I shout into the wind: If the wind Speed = Sound Speed, then I cannot communicate; my voice stops!
- Mass flow reaches a maximum at the throat where  $M=1$   
 → Choked flow.

- Can increase area to get more flow.
- Can change the Reservoir to change flow.

$$M=1 \rightarrow \frac{P_1}{P_2} = \left(\frac{2}{k+1}\right)^{k/k-1} = \underline{\underline{0.53}}$$

$$\frac{T_1}{T_2} = \frac{2}{k+1} = 0.8333 \quad 25^\circ\text{C} \rightarrow -25^\circ\text{C}$$

$$\frac{P_1}{P_2} = \left(\frac{2}{k+1}\right)^{\frac{1}{k-1}} = 0.634$$

- very common in valves, orifices, vacuum systems
  - bike tire → flow is choked through the tire valve
  - = Most Gas Control valves are choked!
- The Choke point is at the minimum Area in The Nozzle / Valve