

## ChE 374–Lecture 20–Pipe Networks

- As we often consider flow in single pipes, pipe networks are the rule not the exception.
- Series and Parallel Pipes.
- Series Flow
  - Total flow rate is constant by mass conservation.
  - Total pressure drop is that through each individual section.
    - \* Includes minor losses.
      - For expansions and contractions, losses “belong” to the smaller pipe.
  - Type I problem: Know D, L, Flow, → get  $\Delta P_L$ .
    - \* Calculate Re, f,  $\Delta P_L$  in each section and add up the pressure losses in each.
  - Type II problem: Know  $\Delta P_L$ , D, L, find  $\dot{V}$ .
    - \* Produce a system demand curve for each pipe:  $\Delta P_L$  vs.  $\dot{V}$ .
    - \*  $\dot{V}$  is constant and  $\Delta P_L = \sum_i \Delta P_{L,i}$ .
    - \* Add the curves vertically to get  $\dot{V}_{tot}$  curve and read off  $\dot{V}_{tot}$  for given pressure loss.
    - \* Or, write equation  $\Delta P_L = \sum_i \Delta P_{L,i}$  explicitly and solve nonlinear equations.
  - Type III or IV problems: Find D or L. This doesn’t count: not unique.
  - Mathcad example for Type II problem.
- Parallel Pipe Networks.
  - Total flow rate is the sum of the flow rates in individual pipes.
  - Pressure drop is the same through each pipe connected to the same two junction points.
  - Type I problem: Flow rate known in a given pipe,  $\Delta P_L$  unknown:
    - \* Compute  $\Delta P_L$  in known pipe as usual, then with  $\Delta P_L$  known in the other pipes, compute flow rate as a usual Type II problem.
  - Type II problem: Pressure drop known, compute flow rates.
    - \* Compute a type II problem in each pipe as usual.
  - Type I problem: Total flow rate known, pressure drop unknown (hard).
    - \* Draw a system demand curve for each pipe. Add horizontally to get the total flow rate versus pressure drop curve. Then for known total flow, pressure drop is known and read off the flow rates through each pipe at that pressure drop. Or, once pressure drop and total flow are known, solve type II problem in each pipe.
    - \* Can also solve system of nonlinear equations, equating pressure drops through each pipe and the expression for pressure drop in terms of flow rate and total flow rate is the sum.
- Can devise complex networks, applying the above principles
  - Like Kirchoff’s laws for electrical networks, but harder since we have nonlinear systems of equations.
    - \* Use a multi-dimensional version of Newton’s method (ChE 541).

## Lecture 20 - Pipe Networks

- Fluid Distribution systems
  - Air - Heating/Cooling
  - water - Cities
  - oil - refineries
- Series / Parallel.
- Similar analysis to electrical Circuits

### Series Flow,



Principles

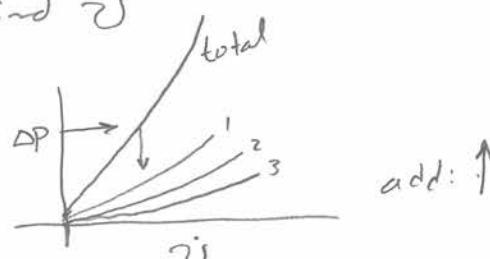
- $\dot{V}$  const by mass conservation  
 $\dot{V}_1 = \dot{V}_2 = \dot{V}_3 = \dot{V}_4$
- $\Delta P_{\text{tot}} = \sum \Delta P_i$
- Expansions / Contractions  $\rightarrow$  eval at the smaller pipe.
- Type I : Know  $L, D, \dot{V} \rightarrow$  Find  $\Delta P$   
 Calc  $Re, f, \Delta P$  in each Section  $\rightarrow$  Sum

- Type II : Know  $\Delta P, D, \text{ find } \dot{V}$

- System Demand Curve

- Read off  $\dot{V}$  from

$\Delta P_{\text{tot}}$  vs  $\dot{V}$  curve, given  $\Delta P_{\text{tot}}$

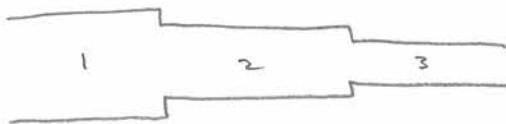


- OR : Solve  $\Delta P_t = \sum_i \frac{L_i \rho V_i^2}{D_e} f_i$  with Colebrook for  $f_i$   
 $\rightarrow$  Solve nonlinear System of eqns,

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- Type III : find  $D$  → Doesn't count, No unique  $D$ ,  
Lots of pipes. (unless know all but one pipe,  
but then its not a network problem)

- Example : 3 pipes :



	$L \text{ (m)}$	$d \text{ (m)}$	$\epsilon \text{ (m)}$
1	100	0.05	0.00024
2	150	0.045	0.00012
3	80	0.04	0.0002

- Find  $v$  for  $\Delta P_t = 320,000 \text{ Pa}$
- Ignore Minor Loss

$$\Delta P_1 + \Delta P_2 + \Delta P_3 = \Delta P_t$$

$$\Delta P_1 = f_L L_1 v_1^2 / 2D_1$$

$$\Delta P_2 = "$$

$$\Delta P_3 = "$$

$$V_x = \frac{v_x}{A_x}$$

$$f_x = f_x(R_{ex}, \epsilon_x/D_x)$$

$$R_{ex} = \rho D_x V_x / \mu$$

Solve system with Matlab: See attached

## Mathcad - [Series\_pipes.xmc d]

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$$\begin{aligned}
 P_t &:= 320000 & p &:= 998 & \mu &:= 1.002 \cdot 10^{-3} & f_1 &:= 0.01 \\
 e_1 &:= 0.00024 & L_1 &:= 100 & D_1 &:= 0.05 & \text{Guesses} & f_2 := 0.01 \\
 e_2 &:= 0.00012 & L_2 &:= 150 & D_2 &:= 0.045 & & f_3 := 0.01 \\
 e_3 &:= 0.0002 & L_3 &:= 80 & D_3 &:= 0.04 & & Q := 0.1
 \end{aligned}$$

Given

$$P_t = f_1 \cdot \frac{L_1}{D_1} \cdot \frac{p}{2} \left( \frac{4Q}{\pi \cdot D_1^2} \right)^2 + f_2 \cdot \frac{L_2}{D_2} \cdot \frac{p}{2} \left( \frac{4Q}{\pi \cdot D_2^2} \right)^2 + f_3 \cdot \frac{L_3}{D_3} \cdot \frac{p}{2} \left( \frac{4Q}{\pi \cdot D_3^2} \right)^2$$

$$\frac{1}{\sqrt{f_1}} + 2 \cdot \log \left[ \frac{e_1}{D_1 \cdot 3.7} + \frac{2.51}{\left( \frac{p \cdot D_1}{\mu} \cdot \frac{4 \cdot Q}{\pi \cdot D_1^2} \right) \cdot \sqrt{f_1}} \right] = 0$$

$$\frac{1}{\sqrt{f_2}} + 2 \cdot \log \left[ \frac{e_2}{D_2 \cdot 3.7} + \frac{2.51}{\left( \frac{p \cdot D_2}{\mu} \cdot \frac{4 \cdot Q}{\pi \cdot D_2^2} \right) \cdot \sqrt{f_2}} \right] = 0$$

$$\frac{1}{\sqrt{f_3}} + 2 \cdot \log \left[ \frac{e_3}{D_3 \cdot 3.7} + \frac{2.51}{\left( \frac{p \cdot D_3}{\mu} \cdot \frac{4 \cdot Q}{\pi \cdot D_3^2} \right) \cdot \sqrt{f_3}} \right] = 0$$

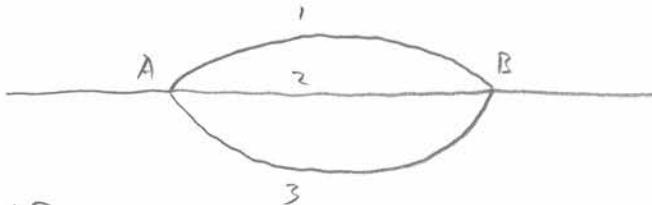
$$\begin{pmatrix} Q \\ f_1 \\ f_2 \\ f_3 \end{pmatrix} := \text{Find}(Q, f_1, f_2, f_3)$$

Re

$$\begin{pmatrix} Q \\ f_1 \\ f_2 \\ f_3 \end{pmatrix} = \begin{pmatrix} 2.64074 \times 10^{-3} \\ 0.03141 \\ 0.02716 \\ 0.03148 \end{pmatrix}$$

## Parallel Pipe Networks.

- Total flow rate is the sum of flow rates in individual pipes.



$$\Delta P_1 = \Delta P_2 = \Delta P_3 \quad \text{Since } P_A \text{ is same for pipes 1, 2, 3.}$$

$P_B$  is same for pipes 1, 2, 3

(easy) • Type I: flow rate known  $\Delta P$  unknown.  
(1 pipe)

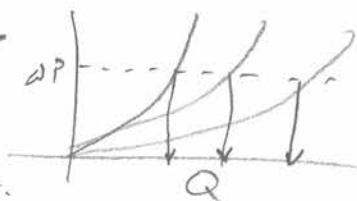
- Compute  $\Delta P$  in known pipe as usual
- Then w/  $\Delta P$ , compute flow rates in other pipes as a Type II problem.

(easy) • Type II:  $\Delta P$  known, flow rates unknown.

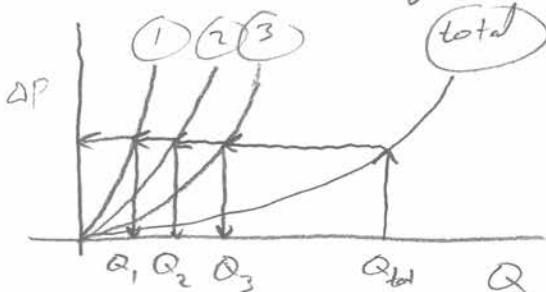
- Compute Type II problem in each pipe  $\rightarrow Q$
- $Q_t = \sum Q_i$

- System Demand Curve for each pipe

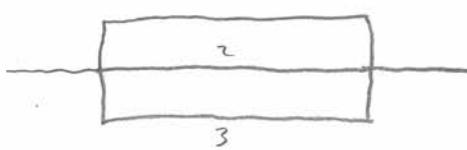
(harder) • Type I: Total flow rate known,  $\Delta P$  unknown.



- System Demand Curve for each pipe.



Or...



$$\begin{array}{l} \textcircled{1} \quad \Delta P_1 = \Delta P_2 \\ \textcircled{2} \quad \Delta P_1 = \Delta P_3 \end{array} \quad \left. \right\} \text{ imply } \Delta P_2 = \Delta P_3.$$

$$\textcircled{3} \quad \Delta P_1 = f_1 \frac{L_1}{D_1} \frac{\rho V_1^2}{2}$$

$$\textcircled{4} \quad \Delta P_2 = f_2 \frac{L_2}{D_2} \frac{\rho V_2^2}{2} \quad \text{use} \quad V_2 = \frac{Q_2}{\frac{\pi}{4} D_2^2}$$

$$\textcircled{5} \quad \Delta P_3 = f_3 \frac{L_3}{D_3} \frac{\rho V_3^2}{2} \quad \text{use} \quad f_3 = f_1 \left( R_{eq}, \frac{D_1}{D_3} \right) \quad \text{w/} \quad R_{eq} = \frac{\pi D_3}{f_1 \frac{Q_3}{\frac{\pi}{4} D_3^2}}$$

$$\textcircled{6} \quad Q_t = Q_1 + Q_2 + Q_3$$

6 eqns in unknowns  $\Delta P_1, \Delta P_2, \Delta P_3, Q_1, Q_2, Q_3$

$$\text{or: } \frac{f_1 L_1}{2 D_1} \rho V_1^2 = f_2 \frac{L_2}{D_2} \frac{\rho V_2^2}{2} \quad \left. \right\}$$

$$\frac{f_1 L_1}{2 D_1} \rho V_1^2 = f_3 \frac{L_3}{D_3} \frac{\rho V_3^2}{2}$$

$$Q_t = Q_1 + Q_2 + Q_3$$

$\rightarrow$  3 eqns in 3 unknowns  
 $Q_1, Q_2, Q_3$

Then, given  $Q$ 's solve for  $\Delta P_1 = \Delta P_2 = \Delta P_3 = f_1 \frac{L_1}{D_1} \frac{\rho V_1^2}{2}$  as a Type 1 problem.

Can easily develop more complex networks

Apply principles to get an equation system.

- at junctions  $\sum Q_i = 0$
- at closed loops  $\sum \Delta P = 0$

Like Kirchhoff's laws but more complex because nonlinear.

- Multi-D Version of Newton's method. M

- Many (commercial) packages

- CHE 541 -

1: conserve mass : Series:  $Q = \text{const}$   
Parallel:  $Q_t = \sum Q_i$  1st-order.

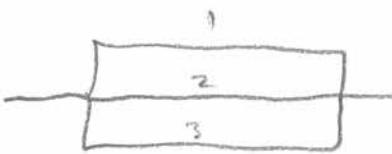
Series:  $\Delta P_t = \sum \Delta P_i$

Parallel:  $\Delta P = \text{Same for branches of 2 nodes}$

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Example

As before, but Parallel not series.



	<u><math>E_1</math></u>	<u><math>L</math></u>	<u><math>D</math></u>
1	0.00024	100	0.05
2	0.00012	150	0.045
3	0.0002	80	0.04

$$\Delta P = ? \quad Q = 0.0133 \text{ m}^3/\text{s.}$$

See Method.

## Mathcad - [Parallel\_pipes.xmcd]

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$Q_t := 0.01333 \quad \rho := 998 \quad \mu := 1.002 \cdot 10^{-3} \quad f_1 := 0.01 \quad Q_1 := 0.004$

$e_1 := 0.00024 \quad L_1 := 100 \quad D_1 := 0.05 \quad \text{Guesses} \quad f_2 := 0.01 \quad Q_2 := 0.004$

$e_2 := 0.00012 \quad L_2 := 150 \quad D_2 := 0.045 \quad f_3 := 0.01 \quad Q_3 := Q_t - Q_1 - Q_2$

$e_3 := 0.0002 \quad L_3 := 80 \quad D_3 := 0.04$

Given

$$f_1 \cdot \frac{L_1 \cdot \rho}{D_1 \cdot 2} \left( \frac{4 \cdot Q_1}{\pi \cdot D_1^2} \right)^2 = f_2 \cdot \frac{L_2 \cdot \rho}{D_2 \cdot 2} \left( \frac{4 \cdot Q_2}{\pi \cdot D_2^2} \right)^2$$

$$f_1 \cdot \frac{L_1 \cdot \rho}{D_1 \cdot 2} \left( \frac{4 \cdot Q_1}{\pi \cdot D_1^2} \right)^2 = f_3 \cdot \frac{L_3 \cdot \rho}{D_3 \cdot 2} \left( \frac{4 \cdot Q_3}{\pi \cdot D_3^2} \right)^2$$

$$\frac{1}{\sqrt{f_1}} + 2 \cdot \log \left[ \frac{e_1}{D_1 \cdot 3.7} + \frac{2.51}{\left( \frac{\rho \cdot D_1}{\mu} \cdot \frac{4 \cdot Q_1}{\pi \cdot D_1^2} \right) \cdot \sqrt{f_1}} \right] = 0$$

$$\frac{1}{\sqrt{f_2}} + 2 \cdot \log \left[ \frac{e_2}{D_2 \cdot 3.7} + \frac{2.51}{\left( \frac{\rho \cdot D_2}{\mu} \cdot \frac{4 \cdot Q_2}{\pi \cdot D_2^2} \right) \cdot \sqrt{f_2}} \right] = 0$$

$$\frac{1}{\sqrt{f_3}} + 2 \cdot \log \left[ \frac{e_3}{D_3 \cdot 3.7} + \frac{2.51}{\left( \frac{\rho \cdot D_3}{\mu} \cdot \frac{4 \cdot Q_3}{\pi \cdot D_3^2} \right) \cdot \sqrt{f_3}} \right] = 0$$

$Q_t = Q_1 + Q_2 + Q_3$

$$\begin{pmatrix} f_1 \\ f_2 \\ f_3 \\ Q_1 \\ Q_2 \\ Q_3 \end{pmatrix} := \text{Find}(f_1, f_2, f_3, Q_1, Q_2, Q_3)$$

$$\begin{pmatrix} f_1 \\ f_2 \\ f_3 \\ Q_1 \\ Q_2 \\ Q_3 \end{pmatrix} = \begin{pmatrix} 0.030663 \\ 0.026613 \\ 0.03118 \\ 5.775203 \times 10^{-3} \\ 3.889447 \times 10^{-3} \\ 3.66535 \times 10^{-3} \end{pmatrix}$$

$$\Delta P := f_1 \cdot \frac{L_1 \cdot \rho}{D_1 \cdot 2} \left( \frac{4 \cdot Q_1}{\pi \cdot D_1^2} \right)^2 \quad \Delta P = 2.647 \times 10^5$$