

Lecture 15 - Dimensional Analysis and Scaling

- Overview:
- Dimensionless groups
 - Example
 - Scaling

Non-dimensionalize an equation

$$\frac{dp}{dt} + \frac{\partial p v}{\partial x} = 0 \quad (=) \quad \frac{\text{kg}}{\text{m}^3 \text{s}} + \frac{\text{kg} \cdot \text{m}}{\text{m}^3 \text{s}} \cdot \frac{1}{\text{m}}$$

- ① each term must have the same units → Dimensional Homogeneity.
- ② Non-Dimensionalize by ÷ eqn by Quantity with the same units of terms.
→ ÷ P/t (or some P/t or equivalent)

Another Π - Group Example

Book - Falling Sphere: $\frac{d^2 z}{dt^2} = -g$ w/ $z = z_0$ at $t = 0$

Params: z, t, g, z_0, V_0
 $m \quad s \quad \frac{m}{s^2} \quad m \quad \frac{m}{s}$

$n_{\text{vars}} = 5$
 $f_{\text{dim}} = 2$ → $k_{\Pi} = 5 - 2 = 3 \text{ } \Pi$'s

Find 3 Π 's: Inspection → $\frac{z}{z_0} = \Pi_1$
 → $t V_0 / z_0 = \Pi_2$

Now need include g

$g (=) \frac{m}{s^2} \div V_0 = \frac{g}{V_0} (=) \frac{1}{s} \times \frac{z_0}{V_0} = \frac{g z_0}{V_0^2} = \Pi_3$

$\Pi_3^{-1/2} = \frac{V_0}{\sqrt{g z_0}} = Fr$

$\Pi_1 = \frac{z}{z_0}$ ratio of lengths

$\Pi_2 = t \frac{V_0}{z_0}$ ratio of times

$\Pi_3 = \frac{g z_0}{V_0^2}$ ratio of inertial and gravity forces.

Note: Can form a time out of $g \rightarrow t \frac{g}{V_0} = \Pi_2$

Can form a length out of $g \rightarrow \frac{z g}{V_0^2} = \Pi_1$

leftovers $\rightarrow \frac{z}{z_0} = \Pi_3$

$\rightarrow \Pi$'s not unique

Scaling: See Slides.

- Recall: Nature does not “know” about our units.
 - kilogram, pounds
 - meters, miles
 - seconds, hours
- Nature only knows about fundamental dimensions, and relative sizes with those dimensions.
 - When we assign values to those dimensions or combinations of those dimensions, we do so relative to our own contrived scales.
 - **Most problems have more natural scales than our units (1 m).**
 - What is the most natural length scale for flow in a room?
 - Then measure length in “room” units $\rightarrow x/L_{\text{room}}$.



How long to cook a roast?

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- How long to cook?
 - Trial and error?
 - Approximate the geometry and properties and solve a heat transfer problem?
 - Solve a complex numerical solution?
- Cookbook Instructions call for **~20 min per lb.**
- Does this make sense? Why or why not?

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"If you roast at 325°F (160°C), subtract 2 minutes or so per pound. If the roast is refrigerated just before going into the oven, add 2 or 3 minutes per pound. ...

"...You thought this was going to be a simple answer, didn't you?"



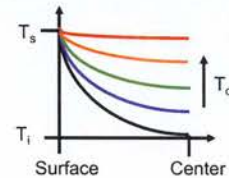
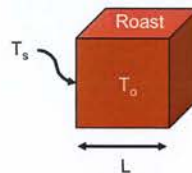
What does the heat equation say?

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$$\frac{\partial T}{\partial t} = -\alpha \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right)$$

$$\frac{\partial T}{\partial t} = -\alpha \left(\frac{\partial^2 T}{\partial x_i^2} \right)$$

$$\alpha = \frac{k}{\rho c_p} \quad (\text{And 1 IC, 2 BCs})$$



- Unsteady heat equation
 - Assuming constant thermal conductivity
 - 3 dimensional, Cartesian coordinates
- Dimensional homogeneity: each term has the same **dimensions** and the same **units**.
 - $k \rightarrow \text{J/s} \cdot \text{m} \cdot \text{K}$; $\rho \rightarrow \text{kg/m}^3$; $c_p \rightarrow \text{J/kg} \cdot \text{K}$; $\alpha \rightarrow \text{m}^2/\text{s}$
- We don't want to solve this equation, just examine it.
- Nondimensionalize, then scale the equation.



Nondimensionalize

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$$\left. \begin{aligned} t^* &= \frac{t}{\tau} \rightarrow t = \tau t^* \\ T^* &= \frac{T - T_{ref}}{T_{ref}} \rightarrow T = T_{ref} T^* + T_{ref} \\ x^* &= \frac{x}{L} \rightarrow x = L x^* \end{aligned} \right\} \rightarrow \frac{\partial T}{\partial t} = -\alpha \left(\frac{\partial^2 T}{\partial x^2} \right) \rightarrow \boxed{\left[\frac{T_{ref}}{\tau} \right] \left(\frac{\partial T^*}{\partial t^*} \right) = - \left[\frac{\alpha T_{ref}}{L^2} \right] \left(\frac{\partial T^*}{\partial x^{*2}} \right)}$$

- Select reference quantities: T_{ref} , L , τ
- Make a direct substitution.
- Simplify: divide through by T_{ref}/τ $\frac{\partial T^*}{\partial t^*} = -\frac{\alpha\tau}{L^2} \left(\frac{\partial T^*}{\partial x^{*2}} \right)$
- Now all terms are nondimensional.
- The group $\alpha\tau/L^2$ is called a dimensionless group and is the Fourier number: a ratio of the physical time to the characteristic diffusion time.



Scaling

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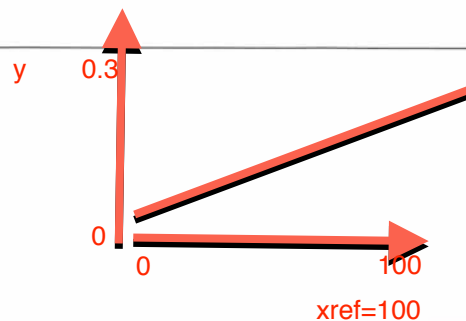
- Now scale the equation:
 - Cengel and Boles call this “normalization”
- If the terms in (...) are $O(1)$, then since the LHS is $O(1)$, the term in [...] must be $O(1)$ also. Then what to choose for τ , L ?
 - L is just the domain size.
 - Then $\tau=L^2/\alpha$
- These are the characteristic scales of the problem.
- Rather than measure length in units of “meters”, nature prefers units of “roast size”

$$\boxed{\left[\frac{T_{ref}}{\tau} \right] \left(\frac{\partial T^*}{\partial t^*} \right) = - \left[\frac{\alpha T_{ref}}{L^2} \right] \left(\frac{\partial T^*}{\partial x^{*2}} \right)}$$

$$\left(\frac{\partial T^*}{\partial t^*} \right) = - \left[\frac{\alpha\tau}{L^2} \right] \left(\frac{\partial T^*}{\partial x^{*2}} \right)$$

“... in the process of scaling, one attempts to select intrinsic reference quantities so that each term in the dimensional equations transforms into the product of a constant factor which closely estimates the term's order of magnitude and a dimensionless factor of unit order of magnitude”

-- Lin and Segal 1988

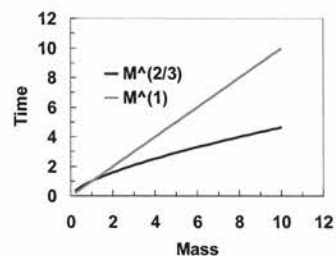


$dy/dx \rightarrow$
 $dy^*/dx^*:$
 $Y^* = y/y_{ref}$
 $x^* = x/x_{ref}$

$dy^* / dx^* = O(1)$

- Now what does this say about cooking a roast?
- The timescale scales as L^2
- But mass scales as L^3

$$\begin{array}{l} \tau \propto L^2 \\ m \propto L^3 \\ \downarrow \\ L \propto m^{1/3} \end{array} \quad \left. \vphantom{\begin{array}{l} \tau \propto L^2 \\ m \propto L^3 \\ L \propto m^{1/3} \end{array}} \right\} \rightarrow \tau \propto m^{2/3}$$



- So cooking time scales with $m^{2/3}$, not with m
- We have not had to solve anything, but we know something valuable about the problem.
 - If you know the time for one roast, you can extrapolate to another.
 - Relationships among parameters!



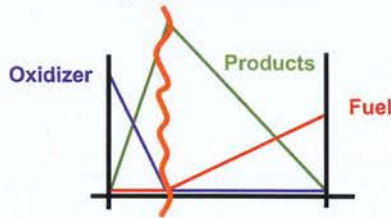
- Nondimensionalization also reduces the number of parameters by showing that they are not independent, but come in characteristic groups.
 - Conduction problem: vary the Fourier number alone, not α and L separately.
 - Book gives simple equation of motion, where initial position, velocity and gravity parameters are collapsed into one parameter, the Froude number.
 - The Fourier number was the ratio of timescales, the Froude number is the ratio of forces.
 - Many others: Friction factor, Drag coefficient, Knudsen number, Mach number, REYNOLDS number.



Scaling Example – One Step Combustion

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Nonpremixed Flames



- Large-scale jet flame simulations: 1-2 weeks on 10,000 processors
- Ethylene combustion with complex chemistry: 19 species and 167 chemical reactions
- Speed setup with a simpler 1-step chemical reaction.
- Reaction characteristics?



Beauty and betrayal in this equation

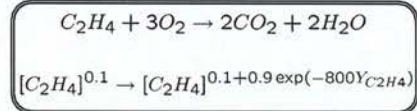
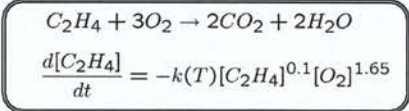
SPECIES

```
H2 CH2 CH3OH AR n-C4H3 C6H3 C5H4OH
H CH2Z C2H N2 i-C4H3 i-C6H4 C5H4O
O CH3 C2H2 CH2CHO C4H4 c-C6H4 C3H8
O2 CH4 C2H3 C3H2 n-C4H5 A1 nC3M7
OH CO C2H4 C3H3 i-C4H5 A1- IC3H7
H2O CO2 C2H5 pC3H4 C4H6 C6H5O C3H6
HO2 HCO C2H6 aC3H4 C4H612 C6H5OH aC3H5
H2O2 CH2O HCCO cC3H4 C4H81 C5H6 CH3CCH2
C CH2OH CH2CO C4H2 C4H7 C5H5 CH3CHO
CH CH3D HCCOH H2C4O C6H2 C5H5O C2H3CHO
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REACTIONS	$k = A T^{-b} \exp(-E/RT)$		
	A	b	E
1. 2O+M ↔ O2+M	1.20E+17	-1.0	0.0
2. O+H+M ↔ OH+M	5.00E+17	-1.0	0.0
3. O+H2 ↔ H+OH	3.87E+04	2.7	6260.0
4. O+HO2 ↔ OH+O2	2.00E+13	0.0	0.0
5. O+H2O2 ↔ OH+HO2	9.63E+06	2.0	4000.0
6. O+CH ↔ H+CO	5.70E+13	0.0	0.0
7. O+CH2 ↔ H+HCO	8.00E+13	0.0	0.0
8. O+CH2Z ↔ H2+CO	1.50E+13	0.0	0.0
9. O+CH2Z ↔ H+HCO	1.50E+13	0.0	0.0
.....			
457. C4H7+H ↔ C4H6+H2	1.80E+12	0.0	0.0
458. C4H7+O2 ↔ C4H6+HO2	1.00E+11	0.0	0.0
459. C4H7+HO2 ↔ CH2O+OH+aC3H5	2.40E+13	0.0	0.0
460. C4H7+HCO ↔ C4H81+CO	6.00E+13	0.0	0.0
481. C4H7+CH3 ↔ C4H6+CH4	1.10E+13	0.0	0.0
462. C2H3+C2H4 ↔ C4H7	7.93E+38	-8.5	14220.0
463. C2H3+C2H5(+M) ↔ C4H81(+M)	1.50E+13	0.0	0.0

Apply Characteristic Timescale

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- **Problem:** Very Stiff Explicit ODE integration
 - Very small timestep sizes required.
 - Takes too many steps.
 - Why?

• Apply Characteristic Timescale

$$\tau = \frac{\Delta[C_2H_4]_{max}}{\left| \frac{d[C_2H_4]}{dt} \right|_{max}} \quad \tau = \frac{[C_2H_4]}{[C_2H_4]^{0.1}} = [C_2H_4]^{0.9}$$

- As $[C_2H_4]$ becomes small, τ becomes small.
- The small reaction order is the culprit.
- Fix: As $[C_2H_4]$ becomes small, increase reaction order.



$$\tau_{new} = [C_2H_4]^{0.9} [1 - \exp(-800Y_{C_2H_4})]$$

